

**F17 - POLYESTER RESIN & FIBERGLASS OPS, FILAMENT WINDING, CLEAN UP SOLVENT, UNCONTROLLED**

**CALCULATION METHODS**

$E_a = U_a \text{ (gal/yr)} \times D \text{ (lbs/gal)} \times \text{Conc. (lbs/lb)} \times \text{MEF} \times (1 - e)$

$E_h = U_h \text{ (gal/hr)} \times D \text{ (lbs/gal)} \times \text{Conc. (lbs/lb)} \times \text{MEF} \times (1 - e)$

**NOTES:**

- Assume no monomers are present in the clean up solvent (i.e . monomer emission rate = 1.0 ).
- Nonvolatile compounds are assumed to have no emissions.
- All volatile organic solvent components used in the clean up are assumed to be fully released.
- Emission calculations are uncontrolled. Capture and removal efficiencies must be identified for controlled processes.

<b>POLLUTANT</b>	<b>AP-42 Default Composition</b>	<b>EPA REFERENCE</b>	<b>EPA</b>	<b>(UNITS)</b>	<b>COMMENTS</b>
	<b>(weight percent)</b>	<b>DOCUMENT</b>	<b>FACTOR</b>		
NOX					
CO					
SOX					
TOG	100.00				Assume TOG = sum of all solvents
ROG	100 - exempts				Assume ROG = TOG - Exempts
TSP					
PM10					
ACETONE					
METHYL METHACRYLATE		Section 4.4 AP-42 (1/95)			- Assume no monomers are present in the clean up solvent (i.e . monomer emission rate = 1.0 ).
STYRENE		Section 4.4 AP-42 (1/95)			- Assume no monomers are present in the clean up solvent (i.e . monomer emission rate = 1.0 ).
TOLUENE					
XYLENES					

Last Updated on 8/26/99  
By D. Byrnes